The Impact of Viscous Dissipation on the Thin Film Unsteady Flow of GO-EG/GO-W Nanofluids

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Abstract: The unsteady flow of nanoliquid film over a flexible surface has been inspected. Water and ethylene glycol are used as the base liquids for the graphene oxide platelets. The comparison of two sorts of nanoliquids has been used for heat transfer enhancement applications. The thickness of the nanoliquid film is kept as a variable. The governing equations for the flow problem have been altered into the set of nonlinear differential equations. The BVP 2.0 package has been used for the solution of the problem. The sum of the square residual error has been calculated up to the 10th order approximations. It has been observed that the graphene oxide ethylene glycol based nanofluid (GO-EG) is more efficient for heat transfer enhancement as compared to the graphene oxide water based nanofluid (GO-W). The impact of the physical parameters has been plotted and discussed.

Keywords: GO-W/GO-EG nanofluids; thin film; unsteady stretching sheet; viscous dissipation; BVP 2.0 package

1. Introduction

Nanofluid is defined as the homogeneous mixture of Nano size particles and base fluid. The thermal conductivity of the standard base fluids, such as oil, ethylene, and water is very small. To improve the thermal efficiency of the base fluid for the enhancement of the heat transfer rate, researchers have immersed the nanoparticles into the base fluid. Choi [1] is the pioneer to introduce the name of the Nano particle. In the field of technology covering chemical production, power stations, and microelectronics, there is a need to recommend new types of fluids that are more active with respect to the heat exchange process. For this reason, Nanofluids are composed to guarantee operative thermal conductivity developments and to achieve the uprising masses of cooling/heating and other materials. Nanofluid is a spreading consisting of nanometer-sized particles (1–100 nm) in size, called nanoparticles. The proper applications of the nanoparticles and the dispersion of the nanoparticles in the base fluid can be seen in the work of Choi et al. [2]. Haq et al. [3] inspected the nanofluid thermal efficiency, over a trapezoidal cavity by using the finite element method. They observed the heated domain partially by increasing the temperature. Soomro et al. [4] analyzed nanoparticle movement over a stretching plate by using passive methods.

Yu et al. [5] found the thermal conductivity and viscosity to discuss the thermal carrying properties of ethylene glycol-based nanofluid. Xie and Chen [6] investigated that idea that the thermal conductivity of the base fluid is much less than that of the graphene oxide nanosheet. To fulfill this space, Xiao et al. [7] tried to model an analytical expression for the thermal conductivity of the nanofluid by using the result of heat convection. Buongiorno [8] studied a complete analysis of the nanofluid. Khan and
Pop [9] investigated the motion of nanofluid by using stretching plate. Shah et al. [10] studied the effects of hall current on steady three-dimensional non-Newtonian nanofluid in a rotating frame with Brownian motion and thermophoresis properties. The thermal conductivity and stability of carbon based nanofluids is very high, visual properties of dynamic surface area, environmental and mechanical stability of carbon-based fluid is satisfactory, due to the electronic hybridization of SP, SP$^2$, SP$^3$. Carbon is an arresting component, graphene is defined as the single coated 2D sheets of graphite. Graphene is mostly used as a nanofluid as the organized potential wall of the solubility is very poor. Thus, we used graphene in the form of graphene oxide (GO), as it changes as a result and forms indisputable dispersion in water due to its high oxidize structure. GO is solvable in oils, the dynamic research area of GO is practically in the rotating disk model of nanofluids. Graphene is a single layer of carbon atom in a hexagonal lattice. The researchers take more interest in graphene oxide as compared to graphene. Graphene oxide (GO) is a two-dimensional material, and it is the oxidized form of graphene with O functional groups. Graphene oxide (GO) was first synthesized in 1859 by Sir Second Baronent Benjamin Colline Brodie via oxidation of bulk graphite with potassium chlorate and nitric acid by chemical method. The natural structure has been studied by Lerf and Klinowsky, at present the most well-known method to synthesize graphene oxide (GO) is the modified hummers method.

The most important application of GO is for industrial machinery and many engineering apparatuses, for example, turbine systems, centrifugal pump rotating blades, turbo machinery hard disk jet motors, and computer storage systems. The central purpose of GO nanofluid flow is the stability of centrifugal forces by engaging the circular pressure gradient. Heat transfer is one of the important properties in chemical processes, which is affected by the base fluid, such as water and mineral oil. The heat transfer properties of mineral oil is lower than water, thus a different method must be used to increase heat transfer, for example: reduced heat transfer or time heat exchangers size can be minimized. Ethylene Glycol (EG) can be used as a cooling fluid and anti-freezing agent to improve thermal properties because the thermal conductivity of the metallic and nonmetallic and carbon structures are much higher than the base fluids.

Balandin et al. [11] studied the single-layer graphene in various base solvents to improve the thermal efficiency of the base fluids. The stable diffusion of the graphene oxide in the ethylene glycol for the enhancement of heat transfer was first analyzed by Wei et al. [12].

Gul et al. [13] investigated the experimental study to examine the stable dispersion of the graphene nanoparticle and to look at the GO-H$_2$O nanofluid by using two rotating discs. Gul et al. [14] examined the water and ethylene glycol-based graphene oxide nanofluid flow under the influence of Marangoni convection. They analyzed the impact of the physical constraints and compared the effect of the embedded parameters using the GO-W and GO-EG nanofluids. The thin film is a thin layer of the fluid having finite domain. Qasim et al. [15] studied heat and mass transfer in nanofluid thin film over an unsteady stretching sheet using Buongiorno’s model.


In this paper, the thin film unsteady flow of GO-EG and GO-W nanofluid in the presence of viscous dissipation have been examined. The comparison of the GO-EG and GO-W have been analyzed under the influence of the physical parameters. The problem has been solved through the optimal homotopy analysis method (OHAM) as described by Liao et al. [22]. This method is frequently used for the solution of nonlinear problems and shows that this method is quickly convergent to the approximate solution. This method is further modified by the Liao [23] for the fast convergence of the nonlinear
problem by introducing the BVP 2.0 package. The researchers [24–30] used this method for the various nonlinear problems occurring in the field of science and engineering.

2. Mathematical Formulation

Consider the unsteady flow of graphene oxide water and ethylene glycol (GO-W/GO-EG) based nanofluids over a flexible sheet. \(U_w = \frac{b\theta}{1-\gamma t}\) is the unsteady flexible velocity of the sheet in the \(x\)-direction, such that \(b, \gamma\) are the positive constants and \(t\) is the term used for the time. The temperature distribution \(T_w(x, t) = T_0 - T_r \left(\frac{b^2}{2\gamma x}\right)(1 - \gamma t)^{-\frac{3}{2}}\) on the surface is supposed to vary with the distance \(x\) from the slit.

The continuity, momentum, and thermal boundary layer equations are settled [15]:

\[
\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \tag{1}
\]

\[
\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \frac{\mu_{uf}}{\rho_{uf}} \frac{\partial^2 u}{\partial y^2} \tag{2}
\]

\[
\frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha_{nf} \frac{\partial^2 T}{\partial y^2} + \frac{\mu_{uf}}{(\rho C_p)_{nf}} \left(\frac{\partial u}{\partial y}\right)^2 \tag{3}
\]

where \(u\) and \(v\) are the velocity component along \(x\) and \(y\) direction, respectively. The associated boundary condition is:

\[
u = U_w, \: \: v = 0, \: \: T = T_w \quad \text{at} \quad y = 0 \tag{4}
\]

\[
\frac{\partial u}{\partial y} = \frac{\partial T}{\partial y} = 0, \: \: v = \frac{\partial h}{\partial t} \quad \text{at} \quad y = \delta, \tag{5}
\]

where \(\delta\) is the film thickness. The similarity transformation is defined as:

\[
\eta = \left(\frac{b}{\nu(1-\gamma t)}\right)^{\frac{1}{2}} y, \: \psi(x, y, t) = \left(\frac{vb}{1-\gamma t}\right)^{\frac{1}{2}} x f(\eta), \: \: T(x, y, t) = T_0 - T_r \left(\frac{b^2}{2\gamma x}\right)(1 - \gamma t)^{-\frac{3}{2}} \theta(\eta) \tag{6}
\]

The stream function \(\psi(x, y)\) is defined as \(u = \frac{\partial \psi}{\partial y}, \: \: v = -\frac{\partial \psi}{\partial x}\), where \(\beta\) is the dimensionless film thickness and is defined as,

\[
\beta = \left(\frac{b}{\nu(1-\gamma t)}\right)^{\frac{1}{2}} h(t) \tag{7}
\]

From Equation (7), we have:

\[
\frac{dh}{dt} = \frac{-\gamma \beta}{2} \left(\frac{\nu}{b}\right)^{\frac{1}{2}} (1 - \gamma t)^{-\frac{1}{2}} \tag{8}
\]

Putting Equation (6) into Equations (2)–(4), and Equation (5), we obtain the following coupled system of ordinary differential equations.

\[
f''' + (1 - \phi)^{2.5} \left[1 - \phi + \phi \frac{\rho_u}{\rho_f}\right] \left[f f'' - (f')^2 - \frac{S}{2} \left(f' + \frac{\eta}{2} f''\right)\right] - (1 - \phi)^{2.5} f' = 0 \tag{9}
\]

\[
\frac{k_{uf}}{k_f} \theta'' + Pr \left(1 - \phi\right) + \phi \left(\frac{\rho C_p}{\rho_f}\right) \left[f \theta' - 2 f' \theta - \frac{S}{2} (3 \theta + \eta \theta')\right] + Ec (f'')^2 = 0 \tag{10}
\]
Here the prime denotes the differentiation with respect to the similarity variable \( \eta \) and dimensionless parameters \( S \), \( Pr \), and \( Ec \) are unsteadiness parameters and defined as:

\[
S = \frac{\gamma}{B}, \quad Pr = \frac{v_{nf}}{\alpha_f}, \quad Ec = \frac{U_0^2}{C_p(T_w - T_0)}
\]

(11)

The transform boundary conditions are,

\[
f(0) = 0, \quad f'(0) = 1, \quad f(\beta) = \frac{S\beta^2}{2}, \quad f''(\beta) = 0, \quad \theta(0) = 1, \quad \theta'(\beta) = 0
\]

(12)

The physical quantities of interest are the skin friction coefficient \( C_{nf} \), and the local Nusselt number \( Nu \), which is defined as,

\[
C_{nf} = \frac{\tau_w}{\frac{1}{2} \rho U_0^2}, \quad Nu = \frac{q_w}{k(T_w - T_0)}\eta
\]

(13)

where \( \tau_w = \mu \left( \frac{\partial \phi}{\partial y} \right)_y = 0, \quad q_w = -k \left( \frac{\partial T}{\partial y} \right)_y = 0 \) and \( q_m = -D_{B} \left( \frac{\partial C}{\partial y} \right)_y = 0 \), are the shear stress heat and mass fluxes at the surface, respectively, using the variables in Equation (7). The associated expressions for dimensionless skin friction coefficient \( C_{nf} \) reduced the Nusselt number \( -\theta' (0) \) and reduced Sherwood number \( -\phi' (0) \) are defined as,

\[
Re_x^{-\frac{1}{2}}C_p = -f''(0), \quad Re_x^{-\frac{1}{2}}Nu_x = -\theta'(0)
\]

(14)

3. Method of Solution

Using the initial estimated values and auxiliary linear operators from Equations (9) and (10),

\[
f_0(\eta) = \frac{3}{2\beta^2} (2 - S) \left[ \frac{x^3}{6} - \frac{\beta x^2}{2} \right] + x, \quad \theta_0(\eta) = 1
\]

(15)

\[
L_f = \frac{d^4 f}{d \eta^4}, \quad L_\theta = \frac{d^2 \theta}{d \eta^2},
\]

(16)

with constant properties:

\[
L_f(C_1 + C_2 \eta + C_3 \eta^2 + C_4 \eta^3) = 0 \quad \text{and} \quad L_\theta(C_5 + C_6 \eta) = 0
\]

(17)

where \( C_i (i = 1, 2, \ldots, 6) \) are arbitrary constants, which are included in general solution.

The average squared residuals error is presented so the Equations (10), (11) and (13) can be written as:

\[
\varepsilon^f_m = \frac{1}{n + 1} \sum_{j=1}^{n} \left[ \kappa_f \left( \sum_{j=1}^{n} f(\eta)_{\eta=\beta \eta} \right) \right],
\]

(18)

\[
\varepsilon^\theta_m = \frac{1}{n + 1} \sum_{j=1}^{n} \left[ \kappa_\theta \left( \sum_{j=1}^{n} \theta(\eta)_{\eta=\beta \eta} \sum_{j=1}^{n} \theta(\eta)_{\eta=\beta \eta} \right) \right],
\]

(19)

\[
\varepsilon^l_m = \varepsilon^f_m + \varepsilon^\theta_m
\]

(20)

4. Table Discussion

Table 1 shows the numerical values of skin friction coefficient for different physical parameters. Here by increasing the value dimensionless film thickness parameter \( \beta \) and unsteady parameter \( S \) the values of skin friction also increase, if we increase the value of unsteady parameter \( S \) the skin friction coefficient value is increased.
Table 1. The numerical values for the skin friction coefficient for different physical parameters when $h = -0.1$, $Pr = 0.7$, $Ec = 0.1, \beta = 0.1$.

<table>
<thead>
<tr>
<th>$\beta$</th>
<th>$S$</th>
<th>$f^{'(0)}$</th>
<th>$f^{'(0)}$</th>
<th>$f^{'(0)}$</th>
<th>$f^{'(0)}$</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td></td>
<td>GO-W $\phi = 0.01$</td>
<td>GO-W $\phi = 0.02$</td>
<td>GO-EG $\phi = 0.01$</td>
<td>GO-EG $\phi = 0.02$</td>
</tr>
<tr>
<td>0.1</td>
<td>0.1</td>
<td>30.3264</td>
<td>30.3335</td>
<td>28.7696</td>
<td>30.4545</td>
</tr>
<tr>
<td>0.2</td>
<td>-</td>
<td>30.3140</td>
<td>30.3412</td>
<td>30.3040</td>
<td>30.3414</td>
</tr>
<tr>
<td>-</td>
<td>0.2</td>
<td>30.2883</td>
<td>30.3261</td>
<td>30.2830</td>
<td>30.3264</td>
</tr>
<tr>
<td>-</td>
<td>0.3</td>
<td>30.7430</td>
<td>28.7777</td>
<td>28.1609</td>
<td>28.7778</td>
</tr>
</tbody>
</table>

Table 2 shows the numerical values of the local Nusselt number for various physical parameters. Here for increasing the values of Prandtl number $Pr$ and unsteady parameter Eckert number $Ec$, the value of local Nusselt number $Nu$ also increases.

Table 2. The numerical values of local Nusselt numbers of different physical parameters, when $\beta = 0.1, h = -0.1, S = 0.1$.

<table>
<thead>
<tr>
<th>$Ec$</th>
<th>$Pr$</th>
<th>$\theta^{'(0)}$</th>
<th>$\theta^{'(0)}$</th>
<th>$\theta^{'(0)}$</th>
<th>$\theta^{'(0)}$</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td></td>
<td>GO-W $\phi = 0.01$</td>
<td>GO-W $\phi = 0.02$</td>
<td>GO-EG $\phi = 0.01$</td>
<td>GO-EG $\phi = 0.02$</td>
</tr>
<tr>
<td>0.1</td>
<td>0.5</td>
<td>-0.1437</td>
<td>-0.4409</td>
<td>-0.6211</td>
<td>-0.4411</td>
</tr>
<tr>
<td>0.2</td>
<td>-</td>
<td>-1.2456</td>
<td>-1.2571</td>
<td>-1.2458</td>
<td>-1.2576</td>
</tr>
<tr>
<td>0.3</td>
<td>-</td>
<td>-1.8697</td>
<td>-1.8869</td>
<td>-1.8700</td>
<td>-1.8875</td>
</tr>
<tr>
<td>-</td>
<td>0.6</td>
<td>0.6026</td>
<td>-1.8337</td>
<td>-0.6027</td>
<td>-0.6098</td>
</tr>
<tr>
<td>-</td>
<td>0.7</td>
<td>0.5870</td>
<td>-1.8875</td>
<td>-0.5871</td>
<td>-0.5952</td>
</tr>
</tbody>
</table>

Tables 3 and 4 represent the individual’s average square residuals error of Water-Graphene Oxide and Ethylene Glycol-Graphene Oxide executed for different order of approximation. We also noticed that the average square residual error value can be reduced by increasing the order of approximation where $m$ represents the number of iterations.

Table 3. Individual averaged squared residual errors for graphene oxide water based nanofluid (GO-W) when $Pr = 6.5$, $Ec = 0.5$, $Nu = 0.1, S = 0.4, \beta = 0.3, \phi = 0.1$.

<table>
<thead>
<tr>
<th>$m$</th>
<th>$\epsilon^2_m$ GO-W</th>
</tr>
</thead>
<tbody>
<tr>
<td>6</td>
<td>$1.7784 \times 10^{-2}$</td>
</tr>
<tr>
<td>12</td>
<td>$9.14122 \times 10^{-4}$</td>
</tr>
<tr>
<td>18</td>
<td>$6.97126 \times 10^{-5}$</td>
</tr>
<tr>
<td>24</td>
<td>$6.44141 \times 10^{-6}$</td>
</tr>
<tr>
<td>30</td>
<td>$6.50496 \times 10^{-7}$</td>
</tr>
</tbody>
</table>

Table 4. Individual averaged squared residual errors for graphene oxide ethylene glycol based nanofluid (GO-EG) when $Pr = 6.5$, $Ec = 0.5$, $Nu = 0.1, S = 0.4, \beta = 0.3, \phi = 0.1$.

<table>
<thead>
<tr>
<th>$m$</th>
<th>$\epsilon^2_m$ GO-EG</th>
</tr>
</thead>
<tbody>
<tr>
<td>6</td>
<td>$1.82761 \times 10^{-2}$</td>
</tr>
<tr>
<td>12</td>
<td>$9.55814 \times 10^{-4}$</td>
</tr>
<tr>
<td>18</td>
<td>$7.39644 \times 10^{-5}$</td>
</tr>
<tr>
<td>24</td>
<td>$6.93791 \times 10^{-6}$</td>
</tr>
<tr>
<td>30</td>
<td>$7.1187 \times 10^{-7}$</td>
</tr>
</tbody>
</table>
5. Result and Discussion

The geometry of the problem is displayed in Figure 1. Figures 2 and 3 indicate the sum of the square residual errors for the velocity pitch and temperature distribution up to the 30th order approximation. These figures show that the convergence of the obtained results is very strong for the proposed problem. These figures show that the increasing order of approximation enhances the convergence rate.

Figure 1. The physical sketch of the problem.

Figure 2. Individual average squared residual errors for EG-W.

Figure 3. Individual averaged squared residual errors for GO-EG.

From Figure 4 we observe that if we increase the amount of the thin film thickness parameter $\beta$, there is an effect on the velocity profile due to increasing $\beta$, meaning that the resistance force increases and consequently the velocity profile decays. In fact, the increasing thickness improves the resistance force and the fluid motion is retarded. The decay effect is comparatively larger in the GO-EG. From
Figure 5 we observe that increasing values of the nanoparticle volume fraction $\phi$ raises the velocity near the sheet surface and the velocity field is delayed after the point of inflection. This effect is comparatively strong in the GO-EG. In fact, the thermophysical properties of the EG is comparatively larger than the water and consequently the increasing value of the nanoparticle volume fraction increases the velocity field.

Figure 5. Effect of dimensional less nanoparticle volume fraction $\phi$ on velocity profile.

Figure 6 shows the effect of the unsteadiness parameter $S$ on the velocity profile. The dimensional axial velocity decreases with increases in the unsteadiness parameter $S$. Actually, the increasing value of $S$ increases the thickness of the momentum boundary layer and consequently the velocity field reduces. This impact is identical for both sorts of nanofluids. Figure 7 indicates the increase in the Prandtl number, thus decreasing the temperature profile. In fact, when the thickness of the momentum boundary layer is larger than that of the thermal boundary layer, or the viscous diffusion is larger than the thermal diffusion, the larger amount of the Prandtl number reduces the thermal boundary layer.

Figure 8 indicates that increasing values of the nanoparticle volume fraction raises temperature. This effect is comparatively strong in the GO-W. In fact, the increasing value of the nanoparticle volume fraction enhances the thermal efficiency of the nanofluid and consequently the temperature field increases. From Figure 9, the relation between the Eckert number and temperature profile is a direct relationship to the physical study of this result, by increasing the Eckert number it will enhance the kinetic energy due to the intermolecular collision and consequently the temperature profile increases. In fact, the viscous dissipation is the key agent in this whole phenomenon and as a result the larger value of the Eckert number enhances the temperature field.
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Figure 6. Effect of the unsteadiness parameter on the velocity profile.

Figure 7. Effect of Prandtl number versus temperature profile.

Figure 8. Effect of dimensionless nanoparticle volume fraction on temperature profile.

Figure 9. Effect of Eckert number on the temperature profile.
6. Conclusions

The thin film of nanofluids over an unstable and flexible sheet has been considered. The GO-W and GO-EG nanofluids have been compared for the heat transfer enhancement applications. The GO-EG nanofluid has stronger thermal conductivity and, therefore, it is concluded that the GO-EG nanofluid is more efficient for the heat transfer enhancement as compared to the GO-W nanofluid. The OHAM technique has been used for the solution of the problem and the strong convergence has been achieved through the residual analysis. The impact of the physical constraints versus the velocity and temperature profiles have been plotted and discussed. The main points are pointed out as:

- By increasing the unsteadiness parameter $S$ the velocity profile decreases and this effect is comparatively strong in the GO-EG nanofluid.
- The increasing value of the Prandtl number reduces the temperature profile. The effect is comparatively strong using the GO-EG nanofluid.
- Increasing the Eckert number increases the kinetic energy to enhance the temperature field.
- The increasing thickness of the thin film reduces the fluid motion.

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Nomenclatures

- $g$: Acceleration due to gravity (ms$^{-2}$)
- $\mu_{nf}$: Dynamic viscosity of the nanofluids axial directions (kgms$^{-1}$)
- $\rho_{nf}$: Density of the nanofluids (kgm$^{-3}$)
- $Ec$: Eckert number ($\frac{U^2}{C_p T_w}$)
- $Q$: Heat generation/absorption parameter (deg)
- $T$: Local temperature (K)
- $\beta$: Non-dimensional thickness of the liquid film
- $Nu$: Nusselt number ($\frac{\rho \nu}{\alpha k_0 T_w}$)
- $Pr$: Prandtl number ($\frac{C_p T_w}{\nu}$)
- $C_p$: Specific heat (Jkg$^{-1}$K$^{-1}$)
- $W_w$: Stretching velocity (ms$^{-1}$)
- $\eta$: Similarity variable ($\frac{u}{\alpha}$)
- $C_f$: Skin friction ($\frac{u}{\alpha}$)
- $\phi$: Solid particle volume fraction
- $\delta$: Thickness of the liquid film
- $T_\delta$: Temperature at the free surface (K)
- $k_{nf}$: Thermal conductivity of the nanoparticles (WM$^{-1}$K$^{-1}$)
- $(u, w)$: Velocity components (ms$^{-1}$)

References


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