Article

Efficient Bacteria Inactivation by Ultrasound in Municipal Wastewater

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Abstract: The reuse of treated wastewaters could contribute to reducing water stress. In this research, ultrasound application on bacterial inactivation in municipal wastewater (MWW) was evaluated. Total and fecal coliforms were used as standard fecal indicators; volatile suspended solids (VSS) were analyzed too. Samples were taken from the effluent of secondary clarifiers. In addition, inactivation tests were carried out on pure cultures of *E. coli* (EC) and *B. subtilis* (BS). Sonication was performed at 20 kHz, 35% amplitude and 600 W/L for 15, 30 and 45 min. After 15 min of sonication, bacterial density was reduced by 1.85 Log_{10} MPN/100 mL for EC and 3.16 Log_{10} CFU/mL for BS. After 30 min, no CFU/mL of BS were observed in MWW and, after 45 min, the reduction of total and fecal coliforms was practically 6.45 Log_{10} MPN/100 mL. Inactivation mechanism was made by cavitation, which causes irreversible damage to the cell wall. Although high bacterial densities were employed, percentages of inactivation >99% were reached at 45 min. This research contributes to the implementation of ultrasound as a disinfection technique with high potential due to its high efficiency without producing byproducts. In fact, the water meets the guidelines for reuse in direct human contact services.

Keywords: cavitation; wastewater; pathogenic contamination; ultrasonic disinfection

1. Introduction

Population and industrial growth demands an intensive use of natural resources. One of them is water supply due to the great magnitude in which it is required. In particular, the use of water resources implies higher levels of pollution due to the generation of wastewaters [1,2]. Nevertheless, treated wastewaters could be used to reduce the water stress generated by the water supply in industrial and/or municipal activities. This is achieved by treating wastewater to meet quality parameters adequate at human and consumption levels [3].

Conventional treatment of municipal wastewater consists of pre-treatment, primary, secondary and tertiary treatment [4]. The last one refers to the disinfection process, where chemical oxidation is the most commonly used through liquid chlorine or gas. However, its major disadvantage is byproducts formation such as trihalomethanes (40–50%), haloacetic acid (28–35%), haloacetonitriles (9–15%) and others (<23%) [5], which are considered toxic and bioaccumulative through the trophic chain. In addition, these byproducts present in wastewater could have negative effects such as acute toxicity, mutagenicity or carcinogenesis in organisms found in water bodies. In addition, chlorine dioxide gas
is the most used, which entails risks to occupational health, since a 1000 ppm concentration causes death within a few minutes of exposure [6].

On the other hand, advanced oxidation processes (AOPs) have demonstrated high removal efficiencies, but with a focus on oxidation of dissolved organic matter, especially persistent organic pollutants [6,7]. One of the most viable is heterogeneous photocatalysis using titanium dioxide or zinc oxides as catalysts. The mechanism of action of this photocatalysis suggests a high technical efficiency in viral and bacterial inactivation. Nonetheless, current designs are laboratory scale and have a great deal of heterogeneity in design, so it is necessary to investigate, in detail, the engineering design, modeling and actinometry to consider large scale operations [8–10].

A viable alternative for disinfection is ultrasound, which is proving to be able to inactivate microorganisms through a series of physical, chemical and mechanical effects derived from cavitation. An advantage of ultrasound disinfection is that bacteria do not develop a resistance against it, or produce toxic byproducts [11–13]. Indeed [11], evaluated the effect of ultrasound on *Escherichia coli* and *Staphylococcus aureus* concentrations in wastewater samples, obtaining a reduction of 2.6 logarithmic units.

The most important operating parameters of the ultrasound application in wastewater disinfection are frequency, amplitude, and sonication time. High values of cell disintegration at frequencies lower than 100 kHz have been shown [13–15]. Amplitude has been found to have a certain proportional correlation with thermal energy in the aqueous medium, causing a greater inactivation of microorganisms. Finally, it is known that sonication time is important in treatment; the longer the sonication time, the greater the microorganisms’ inactivation [11,14,15].

Although several authors have focused on the study of one or more ultrasound operating parameters in the disinfection process [16], the ideal sonication time has not yet been evaluated considering optimal amplitude and frequency conditions and feasibility of being scalable for a municipal wastewater treatment plant [16,17].

Therefore, the objective of this research was to evaluate the ideal sonication time under optimal conditions of frequency and amplitude in samples of conventional municipal wastewater containing total and fecal coliforms. The research was carried out in order to comply with the national and international standards for the reuse of treated wastewaters [18].

2. Materials and Methods

2.1. Samples Selection and Characterization

Ultrasonic disinfection tests were performed on municipal wastewater samples and pure cultures of EC and BS. Municipal wastewater was taken from effluent of secondary settlers of four wastewater treatment plants, which have an activated sludge system as secondary treatment, located in Morelos, México. A total of 39 composite samples were taken every 4 days during six months of sampling following the [19–21] methodology. Fecal and total coliforms, total suspended solids and volatile suspended solids were analyzed in all samples.

Pure cultures tests were performed with *Escherichia coli* ATCC11229, due to it being a bioindicator of fecal contamination in water [21] and with *Bacillus subtilis* ATCC6633, for their differentiation in cell wall. Both microorganisms were evaluated in exponential phase stages, as described in [22,23].

2.2. Microbial Growth Curve

In order to evaluate the application of ultrasound in samples with the highest possible concentration of bacteria, microbial growth curves were determined for reference bacteria: *Escherichia coli* ATCC11229 and *Bacillus subtilis* ATCC 6633. Those curves were carried out in two different stages, pre-inoculum and subsequently in a kinetic study. The pre-inoculum was obtained by inoculating an isolated colony in 100 mL of nutrient broth and was incubated at 37 °C at 120 rpm during 14 h. The second stage consisted of a kinetic study, through an optical density recorder of 1% of
the pre-inoculum in 250 mL of nutritive broth, every 60 min in a spectrophotometer HACH DR5000, Loveland, Co, USA, \( \lambda = 600 \). The method, and their main characteristics used to quantify EC, BS and coliforms are described in Table 1. Finally, the specific growth rate (\( \mu \)) obtained, was calculated relating the biomass amount generated with time. The formula used was indicated in Equation (1).

\[
u = \frac{\ln \frac{X_2}{X_1}}{dt}
\]

where,

- \( X_2 \) = Absorbance corresponding to biomass concentration at time two, nm
- \( X_1 \) = Absorbance corresponding to initial biomass concentration, nm
- \( dt \) = Difference between final and initial time, h.
Table 1. Main characteristics of the methodologies used for quantifying the microorganisms evaluated during sonication tests.

<table>
<thead>
<tr>
<th>Microorganism</th>
<th>Growth Medium</th>
<th>Composition per 1000 mL</th>
<th>Method</th>
<th>Dilution</th>
<th>Temperature for Growth (°C)</th>
</tr>
</thead>
<tbody>
<tr>
<td>B. subtilis</td>
<td>Nutrient Broth, Difco</td>
<td>Meat extract (dehydrated) 3.0 g Peptone 5.0 g</td>
<td>Serial dilutions</td>
<td>$1 \times 10^4 \text{–} 1 \times 10^7$</td>
<td>38</td>
</tr>
<tr>
<td></td>
<td>Nutrient Agar, Difco</td>
<td>Meat extract (dehydrated) 3.0 g Peptone 5.0 g Agar 15.0 g</td>
<td>Spread plate</td>
<td>$1 \times 10^4 \text{–} 1 \times 10^7$</td>
<td>38</td>
</tr>
<tr>
<td>E. coli</td>
<td>Medium EC, Difco</td>
<td>Tryptose 20.0 g Lactose 5.0 g Mixture of bile salts 1.5 g Dibasic potassium phosphate ($K_2HPO_4$) 4.0 g Monobasic potassium phosphate ($KH_2PO_4$) 1.5 g Sodium chloride (NaCl) 5.0 g</td>
<td>Most Probable Number</td>
<td>$1 \times 10^4 \text{–} 1 \times 10^6$</td>
<td>44.5 (Double boiler)</td>
</tr>
<tr>
<td>Total coliforms</td>
<td>Lactose Broth, Difco</td>
<td>Peptone 10.0 g Lactose 10.0 g</td>
<td>Presumptive test</td>
<td>$1 \times 10^4 \text{–} 1 \times 10^6$</td>
<td>38</td>
</tr>
<tr>
<td></td>
<td>Brilliant Green Bile Broth, Merck</td>
<td>Peptone 10.0 g Lactose 10.0 g Ox-bile (dehydrated) 20.0 g</td>
<td>Confirmative test</td>
<td>Only the dilutions that tested positive in the previous test</td>
<td>38</td>
</tr>
<tr>
<td>Fecal coliforms</td>
<td>Lactose Broth, Difco</td>
<td>Peptone 10.0 g Lactose 10.0 g</td>
<td>Presumptive test</td>
<td>$1 \times 10^4 \text{–} 1 \times 10^6$</td>
<td>38</td>
</tr>
<tr>
<td></td>
<td>Medium EC, Merck</td>
<td>Tryptose 20.0 g Lactose 5.0 g Mixture of bile salts 1.5 g Dibasic potassium phosphate ($K_2HPO_4$) 4.0 g Monobasic potassium phosphate ($KH_2PO_4$) 1.5 g Sodium chloride (NaCl) 5.0 g</td>
<td>Confirmative test</td>
<td>Only the dilutions that tested positive in the previous test</td>
<td>44.5 (Double boiler)</td>
</tr>
</tbody>
</table>

Sources: Most Probable Number (MPN) by ISO/DP 9308/2 [24] and Serial dilutions and spread plate by US FDA [24,25].
2.3. Sonication Parameters

Ultrasound equipment used was brand Cole-Parmer model CP505, Vernon Hills, IL, USA, of 200 ± 1.2 W. Optimal frequency and amplitude preliminary tests were performed, considering the operating parameters established in previous studies [26–28]. For that reason, 26 kHz frequency, 20 W/L ultrasonic density and 35% amplitude were set as operating parameters in this investigation. Both parameters have been found in 15, 30, 45 and 60 min of sonication times. It should be noted that all combinations made between amplitude, frequency and sonication time are feasible to scale in a wastewater treatment plant, considering installation, maintenance and operation cost (including energy consumption) [13,29].

2.4. Bacteria Viability during Ultrasound Tests

*E. coli* (*EC*) viability was determined according to the most probable number method (MPN). Besides, *B. subtilis* (*BS*) inactivation was determined by plating serial dilution of the culture. Both methods were carried out in accordance with the standard described in [30–32].

The bacterial suspensions were sonicated using different intensities and frequencies. Samples were taken after 1, 2, 5, 10, and 15 min and analyzed by two methods; counting of colony forming units (CFUs) via plate counting and determination of the fluorescence of fluorescein diacetate absorbed into the bacteria cells (Food Drug Administration analysis). Each determination is the mean of at least three experiments and for the graphical representation the readings were expressed into logarithmic units.

On the other hand, volatile and total solids suspended were determined in the wastewater samples [27,29] during ultrasound application, since both are important for the reuse of treated water, and in particular volatiles refer to the amount of suspended organic matter, in which the microorganisms are the majority content.

2.5. Experimental Design and Statistical Analysis

During experimentation, amplitude and frequency were fixed variables. Thus, statistical treatments were based on two factors: (1) Microorganism type was evaluated with two levels *EC* and *BS*; (2) Sonication time was evaluated with four levels 15, 30, 45 and 60 min. All combinations were performed by triplicate with temperature monitoring. In this regard, experimental design corresponds to a randomized block design, so results were compared through a one-way analysis of variance (One-Way ANOVA), $\alpha = 0.05$. Before ANOVA was made, a normality and homoscedasticity were verified through the Kolmogórov-Smirnov test. All analyses were made in the MINITAB 15 Inc. software, State College, PA, USA.

3. Results and Discussion

3.1. Pure Cultures Standardization of *E. coli* and *B. subtilis*

Growth curve of *EC* as a time function is shown in Figure 1, and linearized tendency to obtain growth rate is represented in Figure 1b; it is observed that Lag phase was reached approximately 1 h after starting the culture, at this time exponential phase began and lasted 4 h, ending 5 h after starting the bacterial culture. Consequently, stationary phase began at 5 h after the start of culture. Based on these results, aliquots for ultrasonic disinfection tests were taken at 4 h after culture started, to guarantee that *EC* cells were in their exponential growth phase. Growth kinetic values match with those reported by [27,32], which indicate a doubling concentration of *EC* every 20 min. In addition, four hours of exponential phase is due because optimal conditions of growing were used for their development (temperature control, oxygenation and medium composition).

Similarly, in Figure 1 the growth of *BS* culture is observed, in which Lag phase is observed during the first two hours, after that exponential phase began and lasted 5 h, which took 7 h of total duration. In this regard, the aliquot evaluated was taken at five hours of process, which is shorter than times reported by [33] in other species of Bacillus and Clostridium genus. The above is due to the fact that
BS metabolizes a wide variety of sugars including xylose, arabinose, malaise, sucrose and glucose, and a wide variety of polymers (proteins and carbohydrates) [34].

3.2. Sampling and Quantification of Coliforms and Suspended Solids

Table 2 shows distribution time of total and fecal coliforms in effluent of secondary clarifier of treatment plant. Daily average was \(1.0 \times 10^6 \pm 1.8 \times 10^5\) MPN/100 mL for total coliforms and \(9.72 \times 10^5 \pm 1.02 \times 10^4\) MPN/100 mL for fecal coliforms. Samples were obtained at 7:00 a.m. in which maximum values were recorded with \(4.06 \times 10^6\) MPN/100 mL for both types of coliforms. This guarantees that obtained results with ultrasound treatment are scalable to the highest microbiological contamination load, values that also coincide with the maximums reported for municipal wastewater [25,35].

On the other hand, Total Suspended Solids (TSS) and Volatile Solids (VSS) average values, in different times (sampling events) are shown in Table 2. The first column refers to the different sampling hours on the same day, established according to the procedures indicated for sampling in wastewater treatment plants [3,4,24].

In all cases, 80% of the TSS was obtained as VSS concentration, which corresponds to conventional municipal wastewater values [3,4]. Therefore, the remaining 20% was considered as inorganic suspended matter, such as clays. In addition, increase in the concentration of coliforms is proportional to the concentration of suspended solids (Table 2). This suggests that suspended solid could be a monitoring parameter during the assessment of ultrasound application in wastewater. Ultrasound application tests were performed on the samples at 7:00 a.m., since they had the highest concentrations of bacteria and suspended solids (Table 2). The results of this assessment are presented in Section 3.3.2.
Table 2. Total and fecal coliforms and suspended matter characterization of secondary effluents of municipal wastewater treatment plants.

<table>
<thead>
<tr>
<th>Sampling Time (h)</th>
<th>Total Coliform (MPN/100 mL)</th>
<th>Fecal Coliform (MPN/100 mL)</th>
<th>Total Suspended Solids, mg/L</th>
<th>Volatile Suspended Solids, mg/L</th>
</tr>
</thead>
<tbody>
<tr>
<td>07:00 a.m.</td>
<td>$4.60 \times 10^6 \pm 2.30 \times 10^5$</td>
<td>$4.60 \times 10^6 \pm 2.30 \times 10^5$</td>
<td>$91.3 \pm 12.3$</td>
<td>$80.7 \pm 10.3$</td>
</tr>
<tr>
<td>10:00 a.m.</td>
<td>$1.50 \times 10^4 \pm 2.60 \times 10^3$</td>
<td>$1.50 \times 10^4 \pm 2.60 \times 10^3$</td>
<td>$57.4 \pm 9.6$</td>
<td>$41.4 \pm 7.6$</td>
</tr>
<tr>
<td>01:00 p.m.</td>
<td>$7.00 \times 10^4 \pm 9.00 \times 10^3$</td>
<td>$4.00 \times 10^4 \pm 4.60 \times 10^2$</td>
<td>$41.2 \pm 5.3$</td>
<td>$33.9 \pm 5.6$</td>
</tr>
<tr>
<td>04:00 p.m.</td>
<td>$2.40 \times 10^5 \pm 9.40 \times 10^3$</td>
<td>$9.30 \times 10^4 \pm 2.30 \times 10^3$</td>
<td>$58.5 \pm 6.8$</td>
<td>$46.1 \pm 7.2$</td>
</tr>
<tr>
<td>07:00 p.m.</td>
<td>$1.50 \times 10^5 \pm 6.20 \times 10^3$</td>
<td>$1.50 \times 10^5 \pm 7.50 \times 10^2$</td>
<td>$81.2 \pm 9.8$</td>
<td>$51.6 \pm 9.4$</td>
</tr>
</tbody>
</table>

3.3. Ultrasound Treatment

3.3.1. Bacterial Inactivation

Table 3 and Figure 2 show general results of ultrasound application to different samples of microorganisms evaluated. After 15 min of sonication, bacterial removal in residual water was $0.11 \log_{10} \text{MPN/100 mL}$ for total coliforms and $0.89 \log_{10} \text{MPN/100 mL}$ for EC with significant differences between them ($p < 0.05$). For pure cultures, the removal efficiency in BS was significantly higher than in EC ($p < 0.05$), since EC was inactivated in $1.85 \log_{10} \text{MPN/100 mL}$ and BS in $3.16 \log_{10} \text{CFU/mL}$. Each of these presented significantly greater inactivation than that obtained for total coliforms and fecal coliforms.

For pure cultures (EC and BS) in growth media, a complete inactivation ($5.92 \log_{10} \text{MPN/100 mL}$ and $6.32 \log_{10} \text{CFU/mL}$) was observed at 30 min of sonication, while for coliforms (total and fecal) present in the wastewater, 45 min of the physicochemical treatment was required for a complete bacterial inactivation.

Table 3. Microorganism average concentration according to ultrasound application at different times.

<table>
<thead>
<tr>
<th>Sonication Time (min)</th>
<th>Coliform</th>
<th>Escherichia coli</th>
<th>Bacillus subtilis</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>Total</td>
<td>Fecal</td>
<td>A B A B A B C D</td>
</tr>
<tr>
<td>0</td>
<td>$2.80 \times 10^6$</td>
<td>$6.45$</td>
<td>$2.80 \times 10^6$</td>
</tr>
<tr>
<td>15</td>
<td>$2.14 \times 10^6$</td>
<td>$6.34$</td>
<td>$3.67 \times 10^5$</td>
</tr>
<tr>
<td>30</td>
<td>$4.83 \times 10^4$</td>
<td>$4.68$</td>
<td>$7.53 \times 10^3$</td>
</tr>
<tr>
<td>45</td>
<td>$&lt;3.00 \times 10^1$</td>
<td>$0.48$</td>
<td>$&lt;3.00 \times 10^1$</td>
</tr>
<tr>
<td>60</td>
<td>$&lt;3.00 \times 10^1$</td>
<td>$0.48$</td>
<td>$&lt;3.00 \times 10^1$</td>
</tr>
</tbody>
</table>

A: MPN/100mL, B: $\log_{10}$ MPN/100 mL, C: CFU/mL, D: $\log_{10}$ CFU/mL.

Figure 2. Treatment with ultrasound at a frequency: 20 kHz, amplitude: 35% and sonication time: 15, 30, 45, 60 min. on (a) total and fecal coliforms, and E. coli and (b) Bacillus subtilis.
The highest time in wastewater treatment is due to the coexistence of around 100 bacterial species, which are more resistant together to sonication treatment [33]. At least four bacteria correspond to coliform genus (Escherichia, Klebsiella, Enterobacter and Citrobacter), and as well other unicellular and pluricellular microorganisms are present, which form a consortium of microorganisms. This consortium in population dynamics causes each microorganism to be more resistant to stress conditions, than if there were only one specie [34–36] as it was observed in pure cultures with EC and BS. In addition, wastewater from secondary clarifier still contains dissolved organic compounds and flocules/aggregates that are also attacked by ultrasound [18]; for that reason it requires higher sonication time to eliminate microorganisms.

Total and fecal coliforms removal at 30 min of sonication were 1.77 \( \log_{10} \) MPN/100 mL and 2.57 \( \log_{10} \) MPN/100 mL respectively with a significance difference between them \( (p < 0.05) \) (Figure 2). The higher inactivation of fecal coliforms may be related to the fact that total coliforms also include genera Klebsiella, Enterobacter and Citrobacter [37,38], which are less susceptible to various disinfecting agents than Escherichia [24,38,39].

Considering that all the genera mentioned above are gram negative bacteria, its cell wall is formed by an outer membrane which is composed of phospholipids that are affected by the increase in temperature modifying its permeability, causing alterations in cellular components and input and output nutrients. It is also important to not forget that at temperatures higher than 60 °C proteins, enzymes and nucleic acids begin to denature [40]. In addition to this, hydroxyl ions and free radicals are generated during the treatment with ultrasound, which act by oxidizing essential components of bacteria (lipids, proteins and genetic material), generating \( \text{H}_2\text{O}_2 \) as a product which is not considered a carcinogen, unlike chlorine disinfection byproducts [14,41,42].

In contrast, gram-positive microorganisms, such as BS, do not have an outer membrane. However, they have a thick layer of peptidoglycan and inside it has a membrane. In the middle of these two walls there is a periplasmic space, in which a greater cavitation is generated by the differences in pressure [42–45], which explains the fact that it presented the highest degree of inactivation compared to EC and both types of coliforms (Figure 2 and Table 3).

Independently of bacterial inactivation percentage, disinfection objective in wastewater treatment is to guarantee public health through complying with established maximum permissible limits (MPL). The main indicators of pathogenic contamination are fecal and total coliforms. In this sense, in Figure 2 it is observed that at 45 min bacterial concentration is below the MPL which are 1000 MPN/100 mL for indirect contact and 240 MPN/100 mL for direct contact [46]. The reduction of microorganisms at 45 min is so effective, that it is microbiologically with the MPL of 2 MPN/100 mL established by [46,47] that refers to water use and human consumption, as well as the guidelines of the World Health Organization for quality of drinking water.

The above indicates that the rupture of bacteria cell wall is caused by cavitation which is related with temperature increasing of the medium, giving rise to a greater permeability of the outer membrane. In fact, in the first 15 min of treatment a temperature of 50 °C was reached, eliminating genus Enterobacter that does not subsist above 40 °C [47]. Subsequently, at 30 min, a temperature of 60 °C was recorded, reaching a maximum of 65 °C from 45 min, which suggests the generation of numerous microbubbles that give rise to repeated implosions, due to the pressure gradient [7,47], in addition to generation of hydroxyl radicals, which have affinity for the compounds with fatty acids that characterize the cell wall [46,47].

Results of bacterial inactivation by ultrasound were similar to those reported by [44], at the same frequency but greater amplitude (35% instead 20%); the same removal percentage was obtained in a shorter time. The above match with the fact that the inactivation of EC is proportional to the increase in amplitude, due to the heat energy generated benefitting the process of bacteria inactivation [13].

Joyce et al., 2003 [14], reported that at 15 min of treatment a complete elimination of gram-positive bacteria was reached, a similar situation to BS in this research. It is important to indicate that operation parameters of frequency at 20 kHz and amplitude at 35% during 45 min were used in this research,
considering in a continuous flow system these parameters are feasible to scale due to the energy consumption it represents [16].

3.3.2. Suspended Solid Removal

TSS and VSS removal as a function of time sonication is observed in Figure 3. Before sonication treatment \( (t = 0) \) VSS proportion was approximately 80% of the TSS. However, this proportion is decreasing as a function of sonication time, which could be related to VSS composition, which are almost entirely microorganisms [3,17]. As explained in the present investigation, sonication causes irreversible damage to the cellular structures of bacteria, in addition to viruses and protozoa, which are precisely those that are quantified together as VSS. In this sense, results indicate the elimination of microorganisms, expressed as SSV, in 52.2, 70.4, 82.7 and 87.6% at 15, 30, 45 and 60 min of sonication respectively (Figure 3).

Despite the fact that residual water samples had been treated by secondary settlers, the ultrasonic treatment allowed to reduce the concentrations until 18% of secondary treatment effluent concentration, complying with the established international values for direct human contact, including irrigation on urban green areas [2,21,25,44]. The high removal efficiencies of suspended solids, despite the low concentration of organic pollutants, is due to the diversity of mechanisms generated by ultrasound in aqueous solutions such as cavitation, shear forces and oxidation by generated hydroxyl radicals [22,46], with the advantage that microorganisms cannot adapt to these mechanisms unlike UV irradiation, and byproducts are not generated as in ozone and chlorination treatment [28,29,45].

![Figure 3. Solid suspended removal by treatment with ultrasound at a frequency: 20 kHz, amplitude: 35% and sonication time: 15, 30, 45, 60 min. TSS = Total suspended solids and VSS = Volatile suspended solid.](image)

3.3.3. Energy Consumption

In addition to the technical feasibility of the ultrasound for bacterial inactivation, it is important to consider the energy consumption of such technology on a large scale. In this sense, and based on the results of the previous sections, a sonication time of 45 min and an applied power of 20 W is considered, which is equivalent to an energy consumption of 12.5 kWh/m³ with the bacteriological characteristics and suspended solids evaluated in the present investigation. For UV disinfection (UVD),
values between 0.5 and 10 kWh/m$^3$ have been reported [48,49] and for ozonation (OZD) between 20 and 100 kWh/m$^3$ [49,50].

The economic cost of using the ultrasound could be from 1.25 to 25 times that of UVD. However, ultrasound does not have the disadvantages of UVD related to the presence of suspended material, which hinders the penetration of light into the water column [48,50,51]. In contrast, the results of the present investigation demonstrated the reduction of suspended solids at the same time as disinfection. Another point to consider is the costs associated with lamp replacement at the UVD, which have a maximum duration of 0.7 years [49], while ultrasound only requires preventive maintenance every six months.

4. Conclusions

The present work contributes to establishing the design and operation parameters necessary for scaling ultrasound technology as a disinfection stage in municipal wastewater treatment trains. In effect, sonication results obtained suggest a cell wall affectation causing its lysis, reaching reductions of up to 6.45 logarithmic units of bacterial density. Sonication treatment reach sufficient water quality values parameters to comply with the maximum permissible limit of 240 MPN/100 mL indicated in the Official Mexican Standard [46], and established by WHO and EPA [2,40], resulting in high quality water suitable for reuse in activities related to direct public contact. In addition, these results were obtained considering high microbiological loads compared to previous studies.

Total inactivation of fecal coliform bacteria was obtained by the conjunction of 30 min of sonication time, 20 kHz frequency and 35% amplitude. Fecal coliform absence in treated wastewater is an indicator of safety for use in activities such as green irrigation areas. Ultrasound application would considerably reduce the demand for drinking water for this activity, and in addition could avoid the use of chemical agents that may be harmful to the health of ecosystems such as chlorine.

Besides, results of suspended solids removal indicate that the ultrasound treatment implementation could be technically feasible due to a significant decrease in the concentration of a wide range of pollutants after secondary treatment [20,21,32], so it is also suggested to evaluate, based on the results of this research, the effect of ultrasound on treated municipal wastewater, considering nitrogen, phosphorus, dissolved organic matter and other more resistant pathogens, such as helminths eggs and in general, physical-chemical monitoring parameters. With the analysis of these results and the analysis of the energy consumption carried out in this work, the technical and economic feasibility of the application of ultrasound on a large scale can be established.

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Author Contributions: Adriana Roé-Sosa and Gabriela E. Moeller-Chávez conceived and designed the experiments; Monserrat Vázquez-Lópezperformed the experiments and analyzed the data; Juan L. García Rojas contributed reagents/materials/analysis tools; Adriana Roé-Sosa wrote the paper and analyzed the statistic section.

Conflicts of Interest: The authors declare no conflict of interest.

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