Kinetic Analysis of the Color of Larch Sapwood and Heartwood during Heat Treatment

Yanxia Wei, Peng Zhang, Yang Liu, Yao Chen *, Jianmin Gao and Yongming Fan

Abstract: The kinetics of color changes in larch sapwood and heartwood during heat treatment were investigated in this study in order to determine if the process of color change that occurs in the surface of wood can be regulated. Wood samples were heated at 90, 110, 130, and 150 °C in an oven, vacuum, and in an oven subjected to saturated steam for 3, 6, 9, and 12 h each. The results of the color measurement showed that the values of $L^*$ (lightness) and $\Delta E^*$ (total color difference) decreased and increased in both the sapwood and heartwood, respectively, with increasing temperature and treatment time. The three kinetic model approach, consisting of (i) the time-temperature superposition principle (TTSP); (ii) zero-order reaction model; and, (iii) first-order reaction model, was used to model the kinetics of color changes. The results indicated that the $L^*$ value of the sample (including heartwood and sapwood) was well fitted to the first-order reaction model ($R^2 = 0.9999$). The Arrhenius activation energy was 14.2369 and 11.0984 kJ/mol for the sapwood and heartwood, respectively. The first-order reaction model also showed a better fit for the $\Delta E^*$ values between sapwood and heartwood with higher $R^2$ values than the other two methods. Therefore, the color changes of larch wood could successfully be analyzed using the first-order reaction model.

Keywords: color change; time-temperature superposition principle (TTSP); zero-order reaction; first-order reaction; kinetics analysis; wood; heat treatment

1. Introduction

Wood color is one of the most important features of wood. Environmental factors (temperature, oxygen, moisture, and sunlight) and the impact of microorganisms are the main reasons for wood discoloration. It can be concluded from previous studies that the color of harvested wood is mainly related to the species [1], genetics [2], aging and weathering [3], drying process [4], the addition of wood preservatives, and chemical and thermal modification processes that are used in wood protection [5]. At present, heat treatment [6] has been widely used to modify harvested wood because it changes the color of wood and improves the apparent performance of wood [7]. Wood becomes darker, and the dimensional stability is improved after heat treatment [8–10]. The intrinsic reason for changes in wood color are mainly related to the chemical composition of wood, especially while taking into account its lignin and extractives [11,12]. The color evolution of heat treated wood is also related to the degradation of hemicelluloses [13] and the modification of the lignin polymer network [14]. Heat treatment results in the degradation of hemicelluloses and the oxidation of extractives in the wood, which produces substances (such as quinone) that cause the wood color to become more yellowish or reddish [15,16]. However, the color of wood became brown when being heated in the higher temperature (180–240 °C) is due to the condensation of polysaccharide by-products in the lignin molecule and the cleavage in $\beta$-O-4 [17–20].
Kinetics studies are generally used to study the color changes in fruits and vegetables, such as chestnuts [21], grapes [22], and rice [23]. The zero- or first-order reaction is suitable for most kinetic analyses, which are mostly applied in the food industry [24]. At a higher temperature, shorter time, and lower temperature over a longer period of time, the same mechanical relaxation phenomenon can be observed, which is referred to as the time-temperature superposition principle (TTSP). The TTSP was originally used to analyze material viscoelasticity [25], and it is widely used to analyze the mechanical properties of wood [26], such as wood creep performance [27–29]. The TTSP was also used in thermal degradation analysis combined with the Arrhenius equation, and it has been used for the determination of the color change of cellulose [30] and wood-plastic composite discoloration analysis [31]. In recent years, model-building methods have also been used in the field of wood thermal discoloration for further examination and experimentation. There has been an increasing number of different models created to study wood color trends during heat treatment [32–34]. In the study of wood thermal discoloration, the Arrhenius equation, while combined with the TTSP [35], is the most commonly used model to predict wood color change. However, the use of zero- and first-order reactions to model the color changes is relatively rare.

Dahurian larch (Larix gmelini) is the main species in the coniferous forest of the Greater Khingan Mountains, China [36]. It is rich in reserves, and it can be used for the raw materials that are necessary for housing construction, civil engineering, and the pole, boat, wood processing, and wood fiber industry. Of all coniferous wood, larch wood has excellent compression strength parallel to the grain and great static bending strength, and it has higher mechanical strength than pine trees. However, there is a clear difference in the color between the heartwood and sapwood of larch wood. The sapwood is light yellow in color, and the heartwood is brown to reddish-brown in color. In the drying process, the inconsistent color changes of sapwood and heartwood may result in uneven surface color of larch wood, which influences its utilization. The application of kinetics is mainly for the process control, like using the correlation between color parameters and heat-treatment intensity for quality control [7,37].

Most of the previous studies only used a method that modeled the color change. Few studies have created a better explanation for the contrast between these different models. The purpose of the current study is to use different heating methods to establish different models for the color change of larch wood, find the optimal kinetic model of larch wood color change, and provide a better theoretical basis for the drying process of larch wood. The color changes in wood drying process can be predicted as a function of time and temperature.

2. Materials and Methods

2.1. Selection and Preparation

Larch wood, aged 20 years, was harvested from northeast China in the Greater Khingan Mountains (E: 121°12′ to 127°00′, N: 50°10′ to 53°33′). A log that was 4 m in length was selected from the middle of the trees. The ratio of sapwood to heartwood was 5:1 with no existence of juvenile wood. The harvested log was 160–200 mm in diameter and 0.56 g/cm³ in basic density, with an initial moisture content of 70%. The log was debarked and cut into discs, with a thickness of 20 mm. The discs were sawed into 20 mm (longitudinal direction) × 50 mm (radial direction) × 20 mm (tangential direction) specimens (including the heartwood and sapwood). The moisture content of the samples was 27.85%, according to the weighing method. The samples were wrapped in plastic wrap and stored in a refrigerator (BCD-190TMPK, Haier refrigerator, Qingdao, Shandong, China) in order to prevent the evaporation of water.

2.2. Heat Treatment

Samples without color defects, knots, and with apparent sapwood and heartwood were carefully selected (for a total of 120 samples). The pretreatment steps of the samples are shown in Figure 1. The sample was completely coated with silica gel and was wrapped with aluminum foil over an
adhesive layer, and then the sample was placed in a Petri dish containing water, with the heartwood positioned so that it was in the water. The water in the Petri dish was continually replenished during the course of the experiment so that the dish never became dry. The equipment that was used to heat the wood in a vacuum was different from the equipment used to heat the wood in an oven and with saturated steam, in view of the low boiling point of water, and this is depicted in Figure 2. The vacuum device was obtained according to the following procedure: (1) the samples were wrapped in aluminum foil and placed in petri dishes, and they were held in place on the dish using a rubber band; (2) the aluminum foil was trimmed off the top of the specimen with a knife so that the dimensions of the aluminum foil were slightly smaller than the top of the wood and it snugly fit; and, (3) the three samples were tightened with a rubber band so that there was firm contact between the dish and the specimen.

![Figure 1](image1.png)

**Figure 1.** The preprocessing of samples heated in an oven and subjected to saturated steam. (a) Original wood sample (including heartwood and sapwood); (b) the wood sample was coated on the outer surface with silica gel and the bottoms of the wood blocks were left open to the air, matching the tops (the white part in Figure 1b); (c) the wood sample was wrapped in aluminum foil (the silver part in Figure 1c) over an adhesive layer; and, (d) the treated heartwood sample was placed in a Petri dish containing water.

![Figure 2](image2.png)

**Figure 2.** The preprocessing of a sample heated in vacuum. (a) The sample were wrapped in aluminum foil and placed in petri dishes; (b) a rubber band was used to hold the samples in place on the dish; and, (c) the aluminum foil was trimmed off the top with a knife.

The samples were heated in an oven at 90, 110, 130, and 150 °C for 3, 6, 9, and 12 h each. The thermal treatment temperatures in vacuum (0.08 MPa) were 90, 110, and in saturated steam were 130 °C, and 110 and 130 °C at the same treatment times. During the heating process, the water in the petri dish was maintained at all times, and a sample was taken every 3 h. All of the samples were removed after 12 h and were dried at atmospheric conditions to a moisture content of 12% for at least 15 days.
2.3. Color Measurement

The initial color parameters were measured for each sample using a Konica Minolta CM-2300d Chroma Meter (Konica Minolta Holdings, Inc., Tokyo, Japan), with a C standard illuminant and 8° standard observer, and simultaneous measurement of SCI (Specular Component Include) and SCE (Specular Component Exclude) was performed. The heated samples were cut into two parts along the center line of the radial direction, and then the color parameters inside the samples were measured. It performed three times of color test on six samples of each specimen. The color parameters $L^*$ (lightness), $a^*$ (green-red coordinate), and $b^*$ (blue-yellow coordinate) were measured for both the sample’s heartwood and sapwood. $\Delta L^*$, $\Delta a^*$, $\Delta b^*$, and $\Delta E^*$ were calculated using the following Equations (1)–(4).

\[
\Delta L^* = L^*_{\text{heated}} - L^*_{\text{unheated}} \\
\Delta a^* = a^*_{\text{heated}} - a^*_{\text{unheated}} \\
\Delta b^* = b^*_{\text{heated}} - b^*_{\text{unheated}} \\
\Delta E^* = \sqrt{(\Delta L^*)^2 + (\Delta a^*)^2 + (\Delta b^*)^2}
\]

where $\Delta L^*$, $\Delta a^*$, $\Delta b^*$, and $\Delta E^*$ represent the changes in the lightness, green/red coordinate, blue/yellow coordinate, and total color difference, respectively. The sapwood and heartwood of the samples were separately and repeatedly measured three times.

2.4. Kinetics Analysis

2.4.1. Arrhenius Equation and the Time-Temperature Superposition Principle

The temperature dependence chemical reaction rates of a substance can be expressed by the Arrhenius equation, according to Equation (5):

\[
k = A \cdot \exp\left(-\frac{E_a}{RT}\right)
\]

where $k$ denotes the reaction rate constant, $A$ denotes the frequency factor, $E_a$ denotes the apparent activation energy, $R$ denotes the gas constant, and $T$ denotes the reaction absolute temperature. The calculation of $E_a$ was obtained by the plot of $\ln(k)\sim1/T$, according Equation (6).

\[
\ln(k) = \ln(A) - \frac{E_a}{RT}
\]

The slope of the Arrhenius curve ($\ln(k)\sim1/T$) is denoted by $E_a$. When the time-temperature equivalence principle (TTSP) is applied to the color change of wood, the same color change can be observed at short-term high temperatures and low temperatures for a long time. The behavior of increasing temperature is equivalent to prolonging the time. A smooth main curve can be obtained by moving the timeline and the color parameter axis. The shift distance of the time and color parameter axis is called the horizontal movement factor $a_T$ (Equation (7)) and the vertical shift factor $b_T$ (Equation (8)), respectively, as shown below:

\[
a_T = \frac{t_T}{t_{ref}} \\
b_T = \frac{P_T}{P_{ref}}
\]

where $t_{ref}$ is the heat treatment time at a reference temperature $T_{ref}$, and $t_T$ is the time that is required to give the same response at temperature $T$. $P_T$ is the color parameter at $T$, and $P_{ref}$ is the color parameter at $T_{ref}$. The calculation of $a_T$ and $b_T$ is based on the reference temperature of 130 °C.
2.4.2. Zero- and First-Order Reaction

The color changes in the wood surface are related to the reaction rate of the various chemical components within the wood. The equation representing the reaction rate is called the kinetic Equation (9):

\[ \frac{dC}{dt} = -kC^n \]  

where \(C\) denotes the quality factor (\(L^*, a^*, b^*, \) and \(\Delta E^*\)); \(n\) denotes the reaction order; \(k\) denotes the reaction rate constant, \(h^{-1}\); and, \(t\) denotes the reaction time, \(h\).

In this study, zero order reactions \((n = 0)\) and first order reactions \((n = 1)\) were used. The kinetic equations are as follows:

zero order reaction : \(kt = C_0 - C\)  

first order reaction : \(kt = \ln(C_0) - \ln(C)\)

where \(C_0\) denotes the initial quality factor.

2.5. Data Processing and Analysis

The mean values of \(L^*, a^*, b^*,\) and \(\Delta E^*\) were calculated for each temperature and time after the data were obtained. The regression analysis of the data was carried out using Origin (Origin 8.5, OriginLab Inc., Washington, DC, USA), Excel (Office 2013, Microsoft, Redmond, WA, USA), 1stOpt (1stOpt 1.5, 7D-Soft High Technology Inc., Beijing, China), and MATLAB (matlab2014a, MathWorks, Natick, MA, USA) software. A second-order polynomial was used to fit the data processed by the Arrhenius equation and the time-temperature superposition principle when using Matlab. The fitted degree of the experimental data and the model was measured using the coefficient of determination \(R^2\) and the root mean square error RMSE as the standard. The values of \(R^2\) that were closer to 1 indicated the better of the fitting model, and the smaller the RMSE, the higher the measurement accuracy.

3. Results and Discussion

3.1. The Color Change during Heat Treatment

Figures 3–5 show the \(L^*, a^*, b^*,\) and \(\Delta E^*\) values of the sapwood and heartwood under different heating conditions. The surface color of the samples became darker after heat treatment. The brightness of the samples showed a decreasing trend with the increasing temperature and time, no matter the heat condition. These results have been verified by researchers such as Santos [38], W Ma [39] and Y Chen [8]. The changes in \(L^*\) of the sapwood decreased from 81.05 to 56.68 when heated in saturated steam (130 °C/12 h), which in heartwood decreased from 75.39 to 58.45. The biggest changes occurred in saturated steam, which indicated that the chemical reaction was greatest in wood that received this treatment. The brightness of sapwood and heartwood was equal, at 68.88 and 68.59, respectively, when the samples were heated in saturated steam (110 °C/12 h). The \(a^*\) and \(b^*\) values increased overall after heat treatment, and these results differ from those of Sugi and Hiba [35]. The change trend of \(a^*\) and \(b^*\) values was different due to the different heat conditions and temperatures, suggesting that the changes in \(a^*\) and \(b^*\) were temperature dependent. The total color difference (\(\Delta E^*\)) increased with the increasing temperature and time, which was pronounced when wood was heated in saturated steam, as opposed to being heated in the oven and vacuum. The \(\Delta E^*\) in sapwood and heartwood increased from 0 to 25.16 and 18.38, respectively, when heated in saturated steam (130 °C/12 h). The changes in sapwood were significant when compared with heartwood, which may be due to the migration with water of the water-soluble extract in the heartwood to the sapwood. The result were also obtained in Araucaria angustifolia [40]. Monotone changes did not occur in the wood that was subject to a vacuum, which may be due to the evaporation of water in the petri dish that resulted in mutative vacuum conditions.
Figure 3. The $L^*$, $a^*$, $b^*$, and $\Delta E^*$ values of the samples that were heated in an oven.
Figure 4. The $L^*$, $a^*$, $b^*$, and $\Delta E^*$ values of the samples that were heated in a vacuum.
Figure 5. The $L^*$, $a^*$, $b^*$, and $\Delta E^*$ values of the samples that were heated in saturated steam.
3.2. Kinetics Analysis

3.2.1. The Time-Temperature Superposition Principle (TTSP)

The changes in the $L^*$ and $\Delta E^*$ values of the samples during the heat treatment were more regular, while the changes in $a^*$ and $b^*$ were relatively cluttered. Therefore, the kinetic analysis of this study was only for the $L^*$ and $\Delta E^*$ of the samples. The smoothly fitted curves of the samples were obtained through the shift of the horizontal shift factor $a_T$ and vertical shift factor $b_T$, which is shown in Figures 6–8. Such a method has also been used to predict the color change during natural aging of Hinoki wood [41]. As shown in Figure 6, the fitted $L^*$ value decreased first and then slightly increased, which was different from the original change trend. However, the changes in the fitted $\Delta E^*$ value for wood heated in an oven were similar to the original change trend. The fitted curve of $L^*$ and $\Delta E^*$ for wood heated in a vacuum and saturated steam was the same as the previous trend (Figures 7 and 8). Therefore, the TTSP method can be used to predict the color changes of samples.

![Figure 6](image1.png)

**Figure 6.** The fitting model using horizontal shift factor $a_T$ and vertical shift factor $b_T$ for $L^*$ and $\Delta E^*$ when samples were heated in an oven.

![Figure 7](image2.png)

**Figure 7.** The fitting model using horizontal shift factor $a_T$ and vertical shift factor $b_T$ for $L^*$ and $\Delta E^*$ when samples were heated in a vacuum.

![Figure 8](image3.png)

**Figure 8.** The fitting model using horizontal shift factor $a_T$ and vertical shift factor $b_T$ for $L^*$ and $\Delta E^*$ when samples were heated in saturated steam.
Table 1 summarizes the $R^2$ values for TTSP fitted to the data set at different heat conditions. The regression lines for the Arrhenius plot showed good linearity ($R^2 > 0.822$) for the hydrothermally treated wood in the treatment temperature range of 70–120 °C [35]. The $R^2$ value was less than 0.9 when the sapwood of the sample was heated in a vacuum, whereas the remaining samples were greater than 0.9. For the sapwood of the sample, the fitted result was $R^2$ (saturation steam) > $R^2$ (oven) > $R^2$ (vacuum), while the heartwood sample was $R^2$ (oven) > $R^2$ (saturation steam) > $R^2$ (vacuum). The fitted effect of the samples that were heated in the vacuum was the worst whether for the sapwood or heartwood. This indicated that the data set for wood treated in a vacuum was not suitable for TTSP. However, the fitted results of the samples under the remaining conditions were greater than 0.95, indicating that it is more optimal to use the TTSP to predict the color change of the samples when they are heated in an oven and are subjected to saturated steam.

### Table 1. The coefficient of determination ($R^2$) and root mean squared error (RMSE) of the samples under different heating conditions by time-temperature superposition principle (TTSP).

<table>
<thead>
<tr>
<th></th>
<th>Oven</th>
<th>Vacuum</th>
<th>Saturated Steam</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>Sapwood</td>
<td>Heartwood</td>
<td>Sapwood</td>
</tr>
<tr>
<td>$L^*$</td>
<td>$R^2$</td>
<td>0.9987</td>
<td>0.9796</td>
</tr>
<tr>
<td></td>
<td>RMSE</td>
<td>0.2769</td>
<td>0.2005</td>
</tr>
<tr>
<td>$\Delta E^*$</td>
<td>$R^2$</td>
<td>0.9641</td>
<td>0.9717</td>
</tr>
<tr>
<td></td>
<td>RMSE</td>
<td>0.2896</td>
<td>0.1884</td>
</tr>
</tbody>
</table>

3.2.2. Zero- and First-Order Reaction

The linear regression analysis was used with the $L^*$ and $\Delta E^*$ values of the samples. The color parameters ($L^*$ and $\Delta E^*$) for the zero-order model are shown in Tables 2 and 3, respectively, and the same parameters for the first-order kinetic model are shown in Tables 4 and 5, respectively.

### Table 2. The regression results from fitting the zero-order model to the $L^*$ value of the samples under different heating conditions.

<table>
<thead>
<tr>
<th></th>
<th>Oven</th>
<th>Vacuum</th>
<th>Saturated Steam</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>90 °C</td>
<td>110 °C</td>
<td>130 °C</td>
</tr>
<tr>
<td>$S$ 1</td>
<td>$k$</td>
<td>0.2638</td>
<td>0.4302</td>
</tr>
<tr>
<td></td>
<td>$R^2$</td>
<td>0.8753</td>
<td>0.9317</td>
</tr>
<tr>
<td></td>
<td>RMSE</td>
<td>0.3781</td>
<td>0.4589</td>
</tr>
<tr>
<td>$H$ 2</td>
<td>$k$</td>
<td>0.2165</td>
<td>0.2513</td>
</tr>
<tr>
<td></td>
<td>$R^2$</td>
<td>0.9458</td>
<td>0.9089</td>
</tr>
<tr>
<td></td>
<td>RMSE</td>
<td>0.2076</td>
<td>0.3040</td>
</tr>
</tbody>
</table>

1 sapwood, 2 heartwood.

### Table 3. The regression results from fitting the zero-order model to the $\Delta E^*$ value of the samples under different heating conditions.

<table>
<thead>
<tr>
<th></th>
<th>Oven</th>
<th>Vacuum</th>
<th>Saturated Steam</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>90 °C</td>
<td>110 °C</td>
<td>130 °C</td>
</tr>
<tr>
<td>$S$ 1</td>
<td>$k$</td>
<td>−0.1538</td>
<td>−0.3044</td>
</tr>
<tr>
<td></td>
<td>$R^2$</td>
<td>0.9298</td>
<td>0.9634</td>
</tr>
<tr>
<td></td>
<td>RMSE</td>
<td>0.1739</td>
<td>0.2172</td>
</tr>
<tr>
<td>$H$ 2</td>
<td>$k$</td>
<td>−0.1624</td>
<td>−0.1716</td>
</tr>
<tr>
<td></td>
<td>$R^2$</td>
<td>0.9942</td>
<td>0.9996</td>
</tr>
<tr>
<td></td>
<td>RMSE</td>
<td>0.0420</td>
<td>0.0106</td>
</tr>
</tbody>
</table>

1 sapwood, 2 heartwood.
Table 4. The regression results from fitting the first-order model to the $L^*$ value of the samples under different heating conditions.

<table>
<thead>
<tr>
<th></th>
<th>Oven</th>
<th>Vacuum</th>
<th>Saturated Steam</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>90 °C</td>
<td>110 °C</td>
<td>130 °C</td>
</tr>
<tr>
<td>$k$</td>
<td>0.0033</td>
<td>0.0054</td>
<td>0.0058</td>
</tr>
<tr>
<td>$R^2$</td>
<td>0.9999</td>
<td>0.9999</td>
<td>0.9999</td>
</tr>
<tr>
<td>RMSE</td>
<td>0.0047</td>
<td>0.0056</td>
<td>0.0054</td>
</tr>
<tr>
<td>$H$</td>
<td>0.0229</td>
<td>0.0334</td>
<td>0.0045</td>
</tr>
<tr>
<td>$R^2$</td>
<td>0.9999</td>
<td>0.9999</td>
<td>0.9999</td>
</tr>
<tr>
<td>RMSE</td>
<td>0.0027</td>
<td>0.0040</td>
<td>0.0044</td>
</tr>
</tbody>
</table>

1 sapwood 2 heartwood.

Table 5. The regression results from fitting the first-order model to the $\Delta E^*$ value of the samples under different heating conditions.

<table>
<thead>
<tr>
<th></th>
<th>Oven</th>
<th>Vacuum</th>
<th>Saturated Steam</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>90 °C</td>
<td>110 °C</td>
<td>130 °C</td>
</tr>
<tr>
<td>$k$</td>
<td>-0.0771</td>
<td>-0.0881</td>
<td>-0.0873</td>
</tr>
<tr>
<td>$R^2$</td>
<td>0.9762</td>
<td>0.9994</td>
<td>0.9988</td>
</tr>
<tr>
<td>RMSE</td>
<td>0.0941</td>
<td>0.0272</td>
<td>0.0384</td>
</tr>
<tr>
<td>$H$</td>
<td>-0.9844</td>
<td>-0.0818</td>
<td>-0.0744</td>
</tr>
<tr>
<td>$R^2$</td>
<td>0.9996</td>
<td>0.9979</td>
<td>0.9988</td>
</tr>
<tr>
<td>RMSE</td>
<td>0.0110</td>
<td>0.0264</td>
<td>0.0262</td>
</tr>
</tbody>
</table>

1 sapwood 2 heartwood.

It can be seen from Tables 2 and 4 that the $k$ value from fitting the zero-order and first-order model to the $L^*$ value increased with the increasing temperature. The reaction rate constant ($k$) for wood heated in saturated steam was significantly larger than that obtained for the other two heating methods, indicating that the temperature and heating conditions have a great effect on the reaction rate of the samples. The larger the value of $k$, the greater the chemical reaction that occurred in the samples, and the greater the corresponding color change, which indicates that the color change that occurred in the wood that was subjected to saturated steam was largest. The $k$ value from fitting the zero-order and first-order model to the $\Delta E^*$ value was irregular when compared with the $L^*$ value, which may have occurred because of the existence of $a^*$ and $b^*$.

$R^2$ reflects the precision of the data set to the fitted model. The larger the $R^2$ value and the lower the value of RMSE, the better the fit degree of the samples. When the zero-order reaction model was used to analyze the $L^*$ value of the samples (Table 2), the regression result $R^2$ for the sapwood was between 0.68 and 0.94, and the heartwood was 0.71 < $R^2$ < 0.96. The RMSE value of the zero-order model with that of TTSP (Table 1) were almost the same. When the $\Delta E^*$ value was fitted (Table 3), the result for sapwood was 0.87 < $R^2$ < 0.99, and the heartwood was 0.91 < $R^2$ < 0.99. The $R^2$ value fitted to $\Delta E^*$ was higher than $L^*$ in general, which demonstrated that the fitted degree of the zero-order model for the $L^*$ value was better than $\Delta E^*$.

The $R^2$ value of the samples was 0.9999 (Table 4) when the first-order reaction model was used to fit the $L^*$ values for linear regression, and the value of RMSE (RMSE < 0.1) was lower than TTSP and zero-order model, which illustrated that the use of the first-order reaction model for $L^*$ was very good. The $R^2$ value of the first-order model for $\Delta E^*$ values (Table 5) was lower than the $L^*$ value, and the majority of wood samples were larger than 0.99, except for the data for the wood heated in vacuum.

When compared with the above four tables, it can be concluded that the $R^2$ (0.9999) for the first-order reaction model was greater than the $R^2$ value ($R^2 < 0.99$) for the zero-order reaction model when the $L^*$ value was fitted; the $R^2$ value for the zero-order model for the $\Delta E^*$ value was lower than the $R^2$ for the first-order reaction model. Therefore, when compared with the zero-order reaction
model, the first-order reaction model (RMSE < 0.1) was more favorable to correctly model the color changes of the samples.

The apparent activation energy (Figures 9 and 10) for change in $L^*$ of the sapwood and heartwood was calculated by the Arrhenius curve on the basis of the zero-order reaction and the first-order reaction. The $E_a$ calculated by the zero-order model for the changes in $L^*$ of the sapwood and heartwood was 13.89 kJ/mol and 10.8597 kJ/mol, respectively, which was 14.2359 kJ/mol (sapwood) and 11.0984 kJ/mol (heartwood) by the first-order reaction. Both of the $E_a$ values are lower than keyaki wood [33] and Hinokiwood [32]. The $R^2$ for the first-order reaction was greater than the zero-order reaction, which corresponded to the previous fitness result, and indicated that the first-order reaction can better express the apparent activation energy of the sample. The $E_a$ of the sapwood was higher than that of the heartwood and it corresponded to the change in the $k$ value between the sapwood and heartwood. The difference in apparent activation energy between the sapwood and heartwood may be related to distinct chemical components [33]. The $E_a$ value calculated by the first-order model was higher than that of the zero-order model, indicating that the reactivity of the chemical composition in the sample represented by the first-order reaction was greater than the reactivity that was represented by the zero-order reaction.

![Arrhenius plots for sapwood](image1.png)

**Figure 9.** Arrhenius plots for $L^*$ of samples in zero-order reaction, and calculated apparent activation energy ($E_a$).

![Arrhenius plots for heartwood](image2.png)

**Figure 10.** Arrhenius plots for $L^*$ of samples in first-order reaction, and calculated apparent activation energy ($E_a$).

### 3.2.3. The comparison of the Three Fitting Models

Tables 6 and 7 summarize the $R^2$ of three kinetic models. In Table 6, the $R^2$ value for the $L^*$ value of the sapwood and heartwood fitted by the first-order models was highest and the zero-order model was the lowest. The $R^2$ for the $\Delta E^*$ was still largest when compared with other methods, while for the
TTSP, it was the worst (Table 7). Therefore, the first-order model was the best model for predicting the color change of sapwood and heartwood.

Table 6. The comparison of $R^2$ values after the fitting of the $L^*$ value using three kinetic models.

<table>
<thead>
<tr>
<th></th>
<th>TTSP</th>
<th>Zero-Order Reaction</th>
<th>First-Order Reaction</th>
</tr>
</thead>
<tbody>
<tr>
<td>Sapwood</td>
<td>$0.8180 &lt; R^2 &lt; 0.9987$</td>
<td>$0.6896 &lt; R^2 &lt; 0.9453$</td>
<td>0.9999</td>
</tr>
<tr>
<td>Heartwood</td>
<td>$0.9528 &lt; R^2 &lt; 0.9796$</td>
<td>$0.7127 &lt; R^2 &lt; 0.9618$</td>
<td>0.9999</td>
</tr>
</tbody>
</table>

Table 7. The comparison of $R^2$ values after the fitting of the $\Delta E^*$ value using three kinetic models.

<table>
<thead>
<tr>
<th></th>
<th>TTSP</th>
<th>Zero-Order Reaction</th>
<th>First-Order Reaction</th>
</tr>
</thead>
<tbody>
<tr>
<td>Sapwood</td>
<td>$0.8352 &lt; R^2 &lt; 0.9974$</td>
<td>$0.8724 &lt; R^2 &lt; 0.9958$</td>
<td>0.9269 &lt; $R^2 &lt; 0.9999$</td>
</tr>
<tr>
<td>Heartwood</td>
<td>$0.9108 &lt; R^2 &lt; 0.9717$</td>
<td>$0.9113 &lt; R^2 &lt; 0.9998$</td>
<td>0.9886 &lt; $R^2 &lt; 0.9998$</td>
</tr>
</tbody>
</table>

4. Conclusions

In this study, larch wood samples were heated in an oven (90, 110, 130, and 150 °C), vacuum (90, 110, and 130 °C), and under saturated steam (110 and 130 °C) for 3, 6, 9, and 12 h each. The color of all the samples was deepened after heat treatment. The color change of sapwood was greater than that of heartwood. The $L^*$ value decreased and the $\Delta E^*$ value increased with increasing temperature and time. The changes in $a^*$ and $b^*$ were temperature dependent and varied in the sapwood and heartwood. The largest changes in $L^*$ and $\Delta E^*$ occurred when wood was heated in saturated steam, and the smallest changes occurred in a vacuum. This may be due to the presence of moisture and oxygen during the heating process, which accelerated the chemical reaction within the samples.

Three types of kinetic models (TTSP, zero-order, and first-order model) were used to analyze the color change. The $R^2$ value for the $L^*$ value ($R^2 = 0.9999$) and $\Delta E^*$ ($R^2 > 0.92$) of the sapwood and heartwood fitted by the first-order models was the highest. The $E_a$ calculated by the first-order model for change in $L^*$ of the sapwood and heartwood was 14.2359 kJ/mol and 11.0984 kJ/mol, respectively. The results signified that the first-order model successfully modeled the color change of the samples. The results of this study can provide predictions for the color change of wood that occurs during the heat treatment process and can serve as a reference for the drying process and color control.

Author Contributions: Y.W., P.Z. and Y.L. conceived, designed and performed the experiments; Y.C., J.G. and Y.F. analyzed the data; all authors wrote the paper.

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